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### PATENT COOPERATION TREAT

### PCT

### **NOTIFICATION OF ELECTION**

(PCT Rule 61.2)

### From the INTERNATIONAL BUREAU

To:

Assistant Commissioner for Patents United States Patent and Trademark Office Box PCT Washington, D.C.20231

in its capacity as elected Office

Date of mailing (day/month/year) 28 February 2000 (28.02.00)

International application No. PCT/EP99/04560

International filing date (day/month/year) 01 July 1999 (01.07.99)

Applicant

JACOBSEN, Claus, J., H. et al

Applicant's	or	agent's	file	reference
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ÉTATS-UNIS D'AMÉRIQUE

PCT-1044-009/co

Priority date (day/month/year) 02 July 1998 (02.07.98)

1.	The designated Office is hereby notified of its election made:
	X in the demand filed with the International Preliminary Examining Authority on:
	19 January 2000 (19.01.00)
	in a notice effecting later election filed with the International Bureau on:
2.	The election X was
	made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland

Authorized officer

C. Villet

Telephone No.: (41-22) 338.83.38

Facsimile No.: (41-22) 740.14.35



## **PCT**

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### INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant's or agent's file reference See Notification of Transmittal of International				otification of Transmittal of International				
PCT-1044-009/co		FOR FURTHER AC	FOR FURTHER ACTION Preliminary Examination					
International application No.		International filing date (c	lay/month/year)	Priority date (day/month/year)				
PCT/EP99/04560 01/07/1999			01/07/1999		02/07/1998			
Internationa C01C1/0		nt Classification (IPC) or na	tional classification and IPC	:				
Applicant HALDOR TOPS E A/S et al.								
HALDOF	IUI	S E AVS et al.		<u>.                                    </u>				
	<ol> <li>This international preliminary examination report has been prepared by this International Preliminary Examining Authority and is transmitted to the applicant according to Article 36.</li> </ol>							
2. This f	REPO	RT consists of a total of	5 sheets, including this	cover sheet.				
b	This report is also accompanied by ANNEXES, i.e. sheets of the description, claims and/or drawings which hav been amended and are the basis for this report and/or sheets containing rectifications made before this Authority (see Rule 70.16 and Section 607 of the Administrative Instructions under the PCT).							
These	ann	exes consist of a total of	1 sheets.					
<u> </u>								
3. This r	eport	contains indications rela	iting to the following iten	ns:				
ı	☒	Basis of the report						
11		Priority						
III   Non-establishment of opinion with regard to novel			pinion with regard to no	velty, inventive s	tep and industrial applicability			
IV		Lack of unity of invention	on					
V	V Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations suporting such statement							
VI		Certain documents cité	ed					
VII 🖾 Certain defects in the international application			nternational application					
VIII	VIII 🖾 Certain observations on the international application							
Date of submission of the demand				Date of completion of this report				
19/01/2000				25.10.2000				
		g address of the internationa	ď	Authorized officer	STON SOFT MICHAEL			
European Patent Office - P.B. 5818 Patentlaan 2  NL-2280 HV Rijswijk - Pays Bas  Tel. +31 70 340 - 2040 Tx: 31 651 epo nl				Zalm, W	The second of th			
Fax: +31 70 340 - 3016				Telephone No. +3	31 70 340 2804			

## INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/EP99/04560

I.	Basi	is f the r port						
1. This report has been drawn on the basis of (substitute sheets which have been furnished to the receiving Officesponse to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed the report since they do not contain amendments.):						shed to the receiving Office in iled" and are not annexed to		
	Des	cription, pages:						
	1-3		as originally	iiled				
	Claiı	ms, No.:						
	1-3	·	as received o	on	27/07/200	00	with letter of	26/07/2000
2.	The	amendments have	e resulted in th	ne cancell	ation of:			
		the description,	pages:					
		the claims,	Nos.:					
		the drawings,	sheets:					
3.					ome of) the amendn as filed (Rule 70.2(c		nts had not been	made, since they have been
4.	Add	itional observation	ns, if necessar	<b>y</b> :				
٧.	Rea app	soned statement licability; citation	t under Article ns and explan	e 35(2) w ations s	ith regard to novel upporting such sta	ty, ite	inventive step ment	or industrial
1.	Stat	ement						
	Nov	etty (N)	Yes: No:	Claims Claims	1-3			
	Inve	entive step (IS)	Yes: No:	Claims Claims	1-3			
	Indu	ustrial applicability	(IA) Yes: No:	Claims Claims	1-3			

2. Citations and explanations

see separate sheet

### VII. Certain defects in the international application

The following defects in the form or contents of the international application have been noted:

see separate sheet

### VIII. Certain observations on the international application

The following observations on the clarity of the claims, description, and drawings or on the question whether the claims are fully supported by the description, are made:

see separate sheet

### **EXAMINATION REPORT - SEPARATE SHEET**

### Re Item V

Reasoned statement under Rule 66.2(a)(ii) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement:

(a) Reference is made to the following documents:

D1: DE-A-2019706 D2: GB-A-2077613

D3: XP002119097 (&SU-A-321045)

(b) The present application does not satisfy the criterion set forth in Article 33(3) PCT because the subject-matter of claims 1-3 does not include an inventive step as defined in the regulations (Rule 65 PCT).

Document D1 describes the preparation of ammonia from hydrogen and nitrogen in presence of a catalyst arranged in a fixed bed and at high pressures (see claim 1). The gas stream flows in a radial mode through the bed. At page 9, last paragraph it is noticed that the particles can have a relative (-for such radial beds-) small diameter: 1 to 3 mm. The process of (amended) claim 1 of the application under consideration differs from this teaching in that (in addition, see item VIII below) particles in the range 0.2-1.5 mm are present in the catalyst bed in about equal amounts in the adjacent size-ranges 0.3-0.8 mm and 0.8-1.5 mm. This feature is considered to result in a higher ammonia product yield (because of an improved flow distribution of the gas through the bed; see page 1, last paragraph of the description).

Document D3 teaches that in a fixéd ammonia synthesis bed the yield can be increased by making use of a catalyst consisting of <u>coarse</u> and <u>small</u> sized (0.5-1.0 mm) particles. The small sized fraction of the catalyst bed of D3 falls within the two ranges as specified in claim 1 of the application under consideration.

With regard to the argument that the catalyst would be present in the reactor in a fluidized state the following is noticed. Although in the title of the abstract the expression 'fluidized bed catalyst' is indeed used it is mentioned in the abstract theat the coarse particles are in a stationary condition whereas the small-sized particles move into the spaces between these coarse particles (see title). The expression 'fluidized bed' should thus be understood as referring to part of the catalyst particles of a bed which as such is static (fixed). A better



expression thus would be 'pseudo-fluidized bed' (this wording is used in the original document). The objectives of the two-size beds disclosed by D3 are similar to those of the process of the present application (increased conversion and less energy consumption). The addition of particles of these sizes (0.5-1.0 mm) to the catalyst known from D1 (1-3 mm) thus appears an obvious measure in order to solve the problem of product yield. The subject-matter of claim 1 is therefore regarded to lack an inventive step.

It is not apparent which part of the application could serve as a basis for a new claim which would satisfy the criteria set forth in Article 33(1) PCT.

### Re Item VII

Certain defects in the international application:

The documents D1,D2 and D3 have not been identified in the description nor has the relevant background art disclosed therein been discussed. The requirements of Rule 5.1(a)(ii) PCT are, thus, not fulfilled.

### Re Item VIII

Certain observations on the international application:

The application does not meet the requirements of Article 6 PCT because the subjectmatter of claims 1 and 2 is not clear.

Claim 1 defines a catalyst composition by the volume ratio of three size ranges present in the powder mixture. The particles in the two lower ranges should each be present in an amount of at least 10% of the mixture. According to claim 2 however the bed contains at least 10 volume-% of the particles in the two lower ranges taken together (claim 2: 'having a size between 0.2 and 1.5 mm').

In case of the argumentation that in addition to the catalyst particles in the three ranges of claim 1 other material is present (so that the two small sized ranges only sum up to less than 10 volume-% of the total including the other material) it appears that the definition of the bed composition is indefinite and should be objected under Article 6 PCT.

International Patent Application No. PCT/EP99/04560

**Applicant: HALDOR TOPSOE A/S** 

PCT 1044-00993/ih Date: July 26, 2000

### **NEW CLAIMS 1 TO 3**

- 1. Process for the preparation of ammonia by contacting an ammonia synthesis gas with ammonia catalyst particles arranged in a fixed bed comprising catalyst particles with a particle size in the range of ≥0.2 mm to <1.5 mm, wherein the fixed bed contains a mixture of catalyst particles with a size of 1.5 3.0 mm, 0.8 1.5 mm and 0.3 0.8 mm in a volume ratio of (40 70):(10 40):(10 30).</p>
- 2. The process of claim 1, wherein the fixed bed contains at least 10% by volume of catalyst particles having a particle size in the range of ≥0.2 mm to <1.5 mm.
- 3. The process of claim 1 or 2, wherein the synthesis gas is passed in radial direction through the fixed bed.